

Clean Development Mechanism in Sewage Treatment Plants

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Abstract: Climate change, currently the biggest threat that the world is facing today has impacts on different sectors such as agriculture, energy, forestry and health. United Nations Framework Conservation on Climate Change was formed to mitigate these threats. Parties to the conservation met at Kyoto, Japan and approved Clean Development Mechanism to combat Green house gas emissions. India has a vast opportunity to explore in terms of CDM and carbon-credits. Through its giant ongoing Infrastructure projects and projects on non-conventional energy sources, a new phase of development is still to be observed, moderate start of which has already begun. One of the projects, which is being applied for CDM is methane collection and utilization from sewage water treatment facilities. The objective of this paper is to identify the size of opportunities for gaining carbon credit through sewage treatment plants.

Keywords --- Biogas, Carbon Credit, CDM, Global Warming, Kyoto Protocol

I. Introduction

1.1 Global Warming

The Earth has an atmosphere of the proper depth and chemical composition. About 30% of incoming energy from the sun is reflected back to space while the rest reaches the earth, resulting in warming the air, oceans, and land, and maintaining an average surface temperature of about 15 °C. The chemical composition of the atmosphere is also responsible for nurturing life on our planet. Most of it is nitrogen (78%); about 21% is oxygen, which all animals need to survive; and only a small percentage (0.036%) is made up of carbon dioxide which plants require for photosynthesis. The atmosphere carries out the critical function of maintaining life-sustaining conditions on Earth, in the following way: each day, energy from the sun is absorbed by the land, seas, mountains, etc. If all this energy were to be absorbed completely, the earth would gradually become hotter and hotter. But actually, the earth both absorbs and, simultaneously releases it in the form of infra red waves. All this rising heat is not lost to space, but is partly absorbed by some gases present in very small (or trace) quantities in the atmosphere, called greenhouse gases (GHGs). Greenhouse gases (for example, carbon dioxide (CO₂), methane (CH₄), nitrous oxide (N₂O), water vapour), re-emit some of this heat to the earth's surface. If they did not perform this useful function, most of the heat energy would escape, leaving the earth cold (about - 18 °C) and unfit to support life.

As the GHGs are transparent to incoming solar radiation, but opaque to outgoing longwave radiation, an increase in the levels of GHGs could lead to greater warming, which, in turn, could have an impact on the world's climate, leading to the phenomenon known as climate change. Indeed, scientists have observed that over the 20th century, the mean global surface temperature increased by 0.6°C

Important greenhouse gases are: water vapour, carbon dioxide (CO₂), methane (CH₄), nitrous oxide (N₂O), hydrofluorocarbons (HFC), perfluorocarbons (PFC), and sulfur hexafluoride (SF₆). Carbon dioxide is used as the benchmark, so all other gases are measured in carbon dioxide equivalence (CO₂e).

Table I
The global warming potential of six major greenhouse gases

Name of the Gas	Global Warming Potential	Atmospheric Life (years)
Water Vapour (H ₂ O)	0.1 to 0.23	Few days
Carbon dioxide (CO ₂)	1	5 to 200
Methane (CH ₄)	21	12
Nitrous oxide (N ₂ O)	310	114
Hydrofluorocarbons (HFC)	140 to 11,700	1.4 to 260
Perfluorocarbons (PFC)	6,500 to 9,200	10,000 to 50,000+
Sulfur hexafluoride (SF ₆)	23,900	3200

1.2 Kyoto Protocol

In 1992 famous Rio earth summit, United Nation Framework Convention on Climate Change (UNFCCC) was adopted with an objective to stabilize atmospheric concentration of GHG at levels that would prevent dangerous humane interference with climate system. The UNFCCC came into effect on 21st March, 1994 according to which industrialized countries shall have the main responsibility to mitigate climate change. Such countries are listed as Annex- I countries. Under UNFCCC all the member countries were to report on their national GHG emissions inventories and propose climate change mitigation strategies. After two and half years of intense negotiation between Annex-I countries, an agreement was struck at the Kyoto protocol on 11 December 1997 in Kyoto, Japan. The convention, participated by 160 countries of the world, was to negotiate binding limitations on greenhouse gases for the developed nations pursuant to the objective of the Framework Convention on Climate Change of 1992.

1.3 Clean Development Mechanism

Under the Kyoto Protocol, emission caps were set for each Annex-I countries, amounting in total to an average reduction of 5.2% below the aggregate emission level in 1990. Each country has a predetermined target of emission reduction as compared to 1990 level. No emission cap is imposed on Non – Annex I countries. However, to encourage the participation of Non-Annex I in emission reduction process a mechanism known as Clean Development Mechanism (CDM) has been provided. The carbon markets are a prominent part of the response to climate change and have an opportunity to demonstrate that they can be a credible and central tool for future climate mitigation. The outcome was the Kyoto Protocol, in which the developed nations agreed to limit their greenhouse gas emissions, relative to the levels emitted in 1990 or pay a price to those that do. At this point comes the carbon trading.

1.4 Carbon Credits

The primary purpose of the Protocol was to make developed countries pay for their ways with emissions while at the same time monetarily rewarding countries with good behaviour in this regard. This system poises to become a big machine for partially transferring wealth from wealthy, industrialised countries to poor, undeveloped countries. A CER or carbon Credit is defined as the unit related to reduction of 1 tonne of CO₂ emission from the baseline of the project activity.

Let us say that India decided to invest in a new power station, and has decided on a particular technology at the cost of X crore. An entity from an industrialised country (which could even be a company) offers to provide India with slightly better technology, which costs more (say Y crore), but will result in lower emissions. The industrialised country will only pay the incremental cost of the project – viz. Y minus X. In return, the investing country will get certified emission reductions (CERs), or credits, which it can use to meet its Kyoto commitments. This is a very good deal indeed – but for the investing country. Not only do they sell developing countries their technology, but they also meet their Kyoto commitments without lifting a finger to reduce their domestic emissions. Countries like the US can continue to pollute at home, so long as it makes the reductions elsewhere.

The World Bank has built itself a role in this market as a referee, broker and macro-manager of international fund flows. The scheme has been entitled Clean Development Mechanism, or more commonly, Carbon Trading.

1.5 CDM Project Types

Type of projects, which are being applied for CDM and which can be of valuable potential, are:

- Energy efficiency projects
 - Increasing building efficiency (Concept of Green Building/LEED Rating)
 - Increasing commercial/industrial energy efficiency (Renovation & Modernization of old power plants)
 - Fuel switching from more carbon intensive fuels to less carbon intensive fuels; and
 - Also includes re-powering, upgrading instrumentation, controls, and/or equipment
- Transport
 - Improvements in vehicle fuel efficiency by the introduction of new technologies
 - Changes in vehicles and/or fuel type, for example, switch to electric cars or fuel cell vehicles (CNG/Bio fuels)
 - Switch of transport mode, e.g. changing to less carbon intensive means of transport like trains (Metro in Delhi); and
 - Reducing the frequency of the transport activity
- Methane recovery
 - Animal waste methane recovery & utilization
- Installing an anaerobic digester & utilizing methane to produce energy
 - Coal mine methane recovery

- Collection & utilization of fugitive methane from coal mining;
 - Capture of biogas
- Landfill methane recovery and utilization
 - Capture & utilization of fugitive gas from gas pipelines;
 - Methane collection and utilization from sewage/industrial waste treatment facilities
- Industrial process changes
Any industrial process change resulting in the reduction of any category greenhouse gas emissions
- Cogeneration
 - Use of waste heat from electric generation, such as exhaust from gas turbines, for industrial purposes or heating (e.g. Distillery-Molasses/ bagasse)
- Agricultural sector
 - Energy efficiency improvements or switching to less carbon intensive energy sources for water pumps (irrigation)
 - Methane reductions in rice cultivation
 - Reducing animal waste or using produced animal waste for energy generation and
 - Any other changes in an agricultural practices resulting in reduction of any category of greenhouse gas emissions

1.6 Indian Scenario- Favouring Points

- a) India - high potential of carbon credits
- b) India can capture 10% of Global CDM market
- c) Annual revenue estimated range from US\$10 million to 330 million
- d) Wide spectrum of projects with different sizes
- e) Vast technical human resource
- f) Strong industrial base

1.7 Biogas Recovery from Sewage Treatment Plants

Biologically produced energy has been identified as an attractive alternative to the increasingly scarce fossil fuel supplies. Resource recovery from waste fetches revenue and makes the environment safe and healthy. Since the Energy Recovery from Sewage Treatment Plants is of the nature of 'non conventional' i.e. 'renewable energy source', it is eco friendly and increases sustainability.

Anaerobic fermentation of organic waste leading to biogas generation is one such process which has considerable potential to supplement energy supplies. Apart from the economic advantages, biogas recycling has great environmental benefits because primary material can be saved and pollution loads from conventionally produced energy can be minimized. The use of renewable energy makes the environment 'clean and green'.

1.8 Direct Benefits of Treatment Plants Designed for Resource Recovery

Sewage treatment plants designed for resource recovery are less expensive to operate than traditional aerobic plants. We need the right kind of sewage treatment. Traditional treatment relies on aerobic micro organisms to convert the organic energy in wastewater to carbon dioxide and biomass (sludge). The process consumes significant amounts of chemicals and electricity, but consuming electrical energy to get rid of organic energy is senseless;

In anaerobic treatment plants on the other hand, methanogenic bacteria digest organic materials and produce raw biogas - a mixture of roughly 1/3 CO₂ and 2/3 methane. When the raw gas is stripped of CO₂ and trace sulphur compounds (using treated wastewater) the resulting natural gas can be used as renewable energy. Anaerobic treatment plants cost less to build since they do not require aeration equipment, and they require less space since they use closed vessels rather than open settling tanks. They also cost less to operate since they do not consume electricity for aeration and use fewer chemicals; aerobic plants require settling agents such as alum and commonly use chlorine to disinfect sludge and effluent. Finally, anaerobic plants produce one fifth to one twentieth of the sludge produced by aerobic plants, since a significant proportion of the energy in the wastewater is converted to methane. Since anaerobic treatment takes place in closed vessels, odours are contained and it becomes practical to co-locate treatment with other land uses.

1.9 Classification of Secondary Treatment

1). Aerobic Treatment Units

a) Suspended Growth

- Activated Sludge Process (ASP),
- Sequencing Batch Reactor (SBR),
- Aerated Lagoon (AL),
- Extended Aeration Process (EA)

■ Membrane Biological Reactors (MBR)

b) Attached Growth

- Trickling Filters (TF),
- Rotating Biological Contactors (RBC),
- Fluidized aerobic bed bioreactors (FAB)

2) *Anaerobic Treatment Units*

a) Suspended Growth:

- Batch Fed (BF),
- Once or Intermittent Fed (OIF),
- Continuous Stirred Reactor -Fed daily with solid recycle (CSR),
- Up-flow Anaerobic Sludge Blanket (UASB),
- Baffle Reactor-Fed daily without solid recycle (BR),
- Continuous Stirred Tank Reactor (CSTR),
- Plug Flow

b) Attached Growth:

- Expanded Bed EB),
- Anaerobic Fluidized Bed (AFB),
- Anaerobic Filters (AF),
- Rotating Biological Disc (RBD)

3) *Aerobic and Anaerobic in Tandem*

- Biofilter

The ASP and UASB based sewage treatment plant are biogas producing plants. The FAB, SBR and WSP based plants are not capable of producing biogas.

1.10 Composition of Biogas

Biogas is a colorless, odorless, inflammable gas, produced by organic waste and biomass decomposition (fermentation). Biogas can be produced from animal, human and plant (crop) wastes, weeds, grasses, vines, leaves, aquatic plants and crop residues etc. The composition of different gases in biogas is as below:

- Methane (CH₄): 55-75%
- Carbon Dioxide (CO₂): 25-45%
- Hydrogen Sulphide (H₂S): 0.1-0.5%
- Nitrogen (N₂): 1-5%
- Hydrogen (H₂): 0-3%
- Carbon Mono Oxide (CO): 0-0.3%
- Oxygen (O₂): Traces

II. Materials and Methods

2.1 Sewage Treatment Plants at Chennai

Chennai Metropolitan Water supply and Sewerage Board (CMWSSB) has been established in 1978 under an Act of Tamil Nadu (Act 28) as a statutory body for exclusively attending to the growing needs and for planned development and appropriate regulation on water supply and sewerage services in the Chennai Metropolitan Area (CMA) in the particular reference to the protection of public health and all the matters connected therewith or incidental thereto. With effective need based and situational management, by adopting opt strategies potable water is being distributed and the used water (sewage) is being collected systematically, pumped to the Sewage Treatment Plant (STP) for safe disposal of the treated sewage to the water ways as prescribed by the PCB thereby the environmental is being not harmed at the same time quality of life of the people also improved.

The wastewater system for the city has been divided into 5 zones; These Zones of macro systems covering the entire City had independent Zonal collections, conveyance, and treatment and disposal facilities.

Table II
Sewage Treatment Plants at Chennai

Zone No	Name of The Zone	Capacity of The Plant (MLD)		
		Old	New	Total
I	Kodunkaiyur	80	110	270
II	Kodunkaiyur	80		
III	Koyumbedu	34	60	94
IV	Nesappakkam	23	40	63
V	Perungudi	-	114	114
	Total	217	324	541

All the plants are of Activated Sludge Process technology. The old plants are not having gas engine facility. The produced gases are simply flared up. Only the new plants having the facility of gas engine which converts the methane in to electricity.

1.2 Quantifying GHG Emission Reductions

Emission reductions are assumed to be the amount of methane that would be emitted during the crediting period in the absence of the agricultural methane Project (minus Project emissions). For each year during the crediting period, Project Proponents shall compare the actual metered methane destruction values and ex-ante modeled estimates of methane destruction. Project Proponents shall claim emission reductions only for the lesser of the two values.

Calculations for Metered Methane Destruction

Tabulated records of total daily agricultural methane gas flows (in standard cubic feet per day) shall be matched with either the continuous methane content data or with the associated periodic reading to methane recovery rates, using Equation 1:

Equation 1: CH₄ Recovered

$$CH_{4\text{recovered}} = B_{\text{Grecovered}} \times \%CH_4$$

Where:

CH₄recovered = Methane recovered per day (as measured in standard ft³/day)

B_{Grecovered} = Biogas recovered per day (as measured in standard ft³/day)

%CH₄ = Methane content of biogas

Methane flows shall be tabulated and summed on a monthly basis using the continuous daily readings for flow and the appropriate methane content readings.

Equation 2: CH₄ Combusted

In order to estimate the amount of methane combusted in metric tons per year (Mg/yr), the annual methane recovery rate in cubic feet per year needs to be converted to weight using Equation 2:

$$CH_{4\text{combusted}} = (CH_{4\text{recovered}} \times 16.04 \times [1/10^6]) \times [1/24.04] \times 28.32 \times DE$$

Where:

CH₄combusted = Annual methane combusted (as measured in Mg/yr)

CH₄recovered = Annual methane recovered (as measured in ft³/yr)

16.04 = molecular weight of CH₄

1/10⁶ = Conversion to metric tons (Mg/g)

1/24.04 = Gas constant (mol/L – measured at standard temperature and pressure – defined as 68F and 14.7psi)

28.32 = Conversion factor (L/cf)

DE = Destruction efficiency of the destruction device (default value of 98%)

Calculation of Project Emissions

Depending on Project-specific circumstances, certain emissions sources may need to be subtracted from total Project emission reductions using the equations below.

Equation 3a: CO₂ Emissions from Fossil Fuel Combustion

$$DestCO_2 = \sum y(FFy * EFy)$$

Where:

DestCO₂ = CO₂ emissions from fossil fuel used in methane destruction process (tCO₂)

FFy = Total quantity of fossil fuel, y, consumed (as measured in volume of fuel)

EFy = Fuel specific emission factor for fuel, y (as measured in tCO₂/fuel quantity - values should be taken from The CCX GHG Emissions Factors online document)

Equation 3b: CO₂ emissions from Project specific electricity consumption

$$Elec CO_2 = (EL_{\text{total}} * EFEL) / 2204.62$$

Where:

- Elec CO₂ = Project specific electricity emissions (tCO₂)
 EL_{total} = Total grid connected electricity consumption (as measured in MWh)
 FEEL = Carbon emission factor for grid electricity (taken from the most recent region specific eGrid values – measured in lbCO₂/MWh) 2204.62 lbCO₂/tCO₂
 Calculation of Project Emission Reductions
 Equation 4: Measured GHG Emission Reductions
 ER = (CH₄combusted * 21) – PE
 Where:
 ER = Total Emission Reductions (tCO₂e)
 CH₄combusted = Annual methane combusted (as measured in Mg/yr)
 21 = Global warming potential of methane
 PE = If applicable, Project emission sources should be subtracted using Equations 3a and 3b

1.3 Reporting and Record-Keeping Requirements

The Project Proponent must maintain all relevant data and documentation related to renewable energy production and monitoring equipment as required. All relevant project documentation shall be kept for a minimum of 2 years beyond each verification time-period.

1.4 Carbon Trading Price

In the United States, some of the companies involved in carbon credit trading are the Chicago Climate Exchange, AgraGate, and the Environmental Credit Corporation. Trading prices have been variable. For the Chicago Climate Exchange, the price per metric ton of CO₂ in 2008 went from \$2 in early 2008 to \$7 in mid-summer, and back to \$2 in the fall

III. Results and Discussions

3.1 Gas Production

Carbon Credit is the function of Methane recovery from the sewage treatment plants. Methane recovery is the function of biogas production. Biogas production is the function of Volatile solids reduction. Volatile solids reduction is the function of Total suspended solids removal. Total suspended solids removal is the function of volume of sludge and method of treatment. Volume of sludge is the function of quantity of waste water. The gas production can be calculated as follows.

- Total suspended solids in the influent = 450 mg/l
 Total suspended solids in the effluent = 30 mg/l
 Total suspended solids removed = 420 mg/l
 Assuming volatile solids to be equal to 70 % of suspended solids, we have
 Volatile solids removed = 70 % X 420 mg/l.
 = 294 mg/l

Now assuming that the volatile solids (matter) is reduced by 65% in the sludge by digestion, we have
 Volatile solids reduced = 65% X 294 = 191.1 mg/l

Therefore Volatile matter reduced per million litre of sewage
 = 191.1 X 10⁶/10⁶ = 191.1 kg

Now assuming that 0.9 m³ of gas is produced per kg of volatile matter reduced, we have, the gas produced/
 million litre of sewage

$$= 0.9 \times 191.1 = 171.99 \text{ m}^3 \text{ (or) } = 172 \text{ m}^3$$

3.2 Calorific Value of Biogas

CH₄=65vol%; CO₂=32vol%

Calorific value of pure CH₄ = 50,000kJ/kg

Calorific value of biogas

(0.65 X 16 X 50,000) / (0.65 X 16 + 0.32 X 44)

$$= 21241.8 \text{ kJ/kg} = 21.24 \text{ MJ/kg}$$

Avg. mole wt.

$$= 0.65 \times 16 + 0.35 \times 44$$

$$= 25.8 \text{ kg/k.mole}$$

Volume per unit weight

$$= 22.414 / \text{mol wt. (m}^3/\text{kg)}$$

$$= 22.414 / 25.8$$

$$= 0.8688 \text{ m}^3/\text{kg}$$

C.V. of biogas

$$= 21241.8 \text{ kJ/kg}$$

$$= 21241.8 / 0.8688 \text{ [(kJ/kg) / (m}^3/\text{kg)]}$$

(m³/kg)]

$$= 24450 \text{ kJ/ m}^3$$

Projected Electricity

$$= 24450 / 3600 \text{ [1J=1 watt sec]} = 6.792 \text{ kWh/ m}^3$$

Efficiency of Gas engine, η = 30%,

Actual Electricity

$$= 6.792 \times 0.30$$

$$= 2.04 \text{ kWh/ m}^3$$

C. Power Generation as Per the Production of Biogas

Table III
Theoretical gas production
Gas produced per million litre of sewage = 172 m³

Sl.No	Location of STP	Capacity in MLD	Theoretical gas production in m ³
1	Kodunkaiyur	110	18920
2	Koyambedu	60	10320
3	Nesappakkam	40	6880
4	Perungudi	114	19608
	Total	324	55728 m ³

Table IV
Energy Production from Biogas Energy production for 1 m³ biogas @ 21.24 MJ/m³ = 2.04 kWh

Sl. No	Location of STPs	Biogas production in m ³	Energy production /day MWh/day
1	Kodunkaiyur	18920	38.60
2	Koyambedu	10320	21.05
3	Nesappakkam	6880	14.04
4	Perungudi	19608	40.00
Total Energy production per day MWh/day			113.69 MWh
Annual Electricity Production: 113.69 MWh X 270 days (9)			30696 MWh
Total Electricity savings per year@ Rs4.20 per unit			Rs. 1289.00 lakhs

3.3 Calculations for Metered Methane Destruction

Equation 1:

$$\text{CH}_4\text{recovered} = \text{B}_{\text{Grecovered}} \times \% \text{CH}_4$$

$$\text{CH}_4\text{recovered} = 55728 \text{ m}^3 \times 0.65 = 36223 \text{ m}^3 * 35.32 \text{ cft} = 1279396 \text{ ft}^3/\text{day}$$

$$\text{Due to seasonal variation, only 270 days in an year will be taking into account} = 1279396 * 270 = 345436920 \text{ ft}^3/\text{year}$$

Equation 2:

$$\text{CH}_4\text{combusted} = (\text{CH}_4\text{recovered} \times 16.04 \times [1/106] * [1/24.04] \times 28.32) * \text{DE}$$

$$\text{CH}_4\text{combusted} = (345436920 \text{ ft}^3 \times 16.04 \times [1/10^6] * [1/24.04] \times 28.32) * 0.98 = 6396.73$$

metric tons per year

Calculation of Project Emissions

Depending on Project-specific circumstances, certain emissions sources may need to be subtracted from total Project emission reductions using the equations below.

Equation 3a:

CO₂ Emissions from Fossil Fuel Combustion

$$\text{DestCO}_2 = \sum y(\text{FF}_y * \text{EF}_y) = \text{Zero}$$

(since there will be no Fossil Fuel required for the biogas conversion)

Equation 3b:

CO₂ emissions from Project specific electricity consumption

$$\text{Elec CO}_2 = (\text{EL}_{\text{total}} * \text{EF}_{\text{EL}}) / 2204.62 = \text{Zero} \text{ (since there will be no electricity required for the biogas conversion)}$$

Calculation of Project Emission Reductions

Equation 4:

Measured GHG Emission Reductions

$$\text{ER} = (\text{CH}_4\text{combusted} * 21) - \text{PE}$$

$$\text{ER} = (6396.73 * 21) = 134331.33 \text{ metric tons per year}$$

$$\text{Carbon Trading price} = \$2 \text{ per metric tons} * 134331.33$$

$$= \$ 268663$$

3.4 Carbon Trading Opportunities in India

The total waste water generation in class I cities is 16,662.5 MLD. As per Indian conditions, the minimum total suspended solids in the influent are 200mg/l. and the maximum total suspended solids in the influent are 500 mg/l. So, taking average total suspended solids in the influent as 350 mg/l; Total suspended solids in the influent is 350 mg/l; Total suspended solids in the effluent is 30 mg/l. & Total suspended solids removed is 320 mg/l.

Assuming volatile solids to be equal to 70 % of suspended solids,

$$\begin{aligned} \text{We have Volatile solids removed} &= 70 \% \times 320 \text{ mg/l.} \\ &= 224 \text{ mg/l.} \end{aligned}$$

Now assuming that the volatile solids (matter) is reduced by 65% in the sludge by digestion, we have Volatile solids reduced

$$\begin{aligned} &= 65\% \times 224 \\ &= 145.6 \text{ mg/l.} \end{aligned}$$

$$\begin{aligned} \text{Therefore Volatile matter reduced / million litre of sewage} \\ &= 145.6 \times 10^6 / 10^6 \\ &= 145.6 \text{ kg} \end{aligned}$$

Now assuming that 0.9 m³ of gas is produced / kg of volatile matter reduced, we have

$$\begin{aligned} \text{The gas produced per million litre of sewage} \\ &= 0.9 \times 145.6 \\ &= 131.04 \text{ m}^3 \text{ (or)} \\ &= 131 \text{ m}^3 \end{aligned}$$

The total waste water generation in class I cities is 16,662.5 MLD.

$$\begin{aligned} \text{Biogas production} &= 16,662.5 \times 131 \\ &= 2182787.5 \text{ m}^3 \end{aligned}$$

Considering one-fourth of the volume, we have, 545697 m³ of biogas production.

$$\begin{aligned} \text{Biogas production} &= 545697 \text{ m}^3 \\ \text{C.V. of Biogas} &= 21.24 \text{ MJ/kg} \\ \text{Energy production for 1 m}^3 \text{ biogas} &@ 21.24 \text{ MJ/ m}^3 \\ &= 2.04 \text{ kWh/day} \end{aligned}$$

$$\begin{aligned} \text{Energy production per day} &= 545697 \times 2.04 \\ &= 1113221.88 \text{ kWh/day} \\ &= 1113.22 \text{ MWh/day. (Say)} \\ &= 1100 \text{ MWh/day} \end{aligned}$$

$$\begin{aligned} \text{Annual Power Production: } &1100 \text{ MWh} \times 270 \text{ days} \\ &= 297000 \text{ MWh @ Rs. 4.00 per unit (average), total Electricity savings per} \\ \text{year} &= 297000 \times 4.00 \times 1000 \\ &= \text{Rs. 118.80 crores.} \end{aligned}$$

$$\begin{aligned} \text{CH}_4 \text{ recovered} &= 545697 \text{ m}^3 \times 0.65 = 354703 \text{ m}^3 \times 270 \\ &= 95769810 \text{ m}^3 \text{ / year} \end{aligned}$$

$$\begin{aligned} \text{CH}_4 \text{ combusted} &= (95769810 \text{ m}^3 \times 35.32 \times 16.04 \times [1/10^6]) \times [1/24.04] \times 28.32 \times 0.98 \\ &= 62638.10 \text{ metric tons per year} \end{aligned}$$

$$\begin{aligned} \text{GHG Emission Reductions ER} &= 62638.10 \times 21) \\ &= 1315400.1 \text{ metric tons per year} \end{aligned}$$

$$\begin{aligned} \text{Carbon Trading price} &= \$2 \text{ per metric tons} \times 1315400.1 \\ &= \$ 2630800 \end{aligned}$$

IV. Conclusion

Sewage treatment plants designed for resource recovery are less expensive to operate than traditional aerobic plants. We need the right kind of sewage treatment. The ASP and UASB based sewage treatment plant are biogas producing plants. The FAB, SBR and WSP based plants are not capable of producing biogas.

Chennai city has a total sewage treatment capacity of 541MLD. All the plants are equipped with Activated Sludge Process technology. Out of which, only 324 MLD capacity of plants are having biogas conversion technology. 217 MLD of plants are old plants and are not having the technology of biogas conversion. From the available technology, the theoretical CER per annum is 134331.33 metric tons. Assuming the Carbon Trading price as \$2 per metric tons, we can earn \$ 268663 per year.

The total waste water generation in class I cities is 16,662.5 MLD. Considering one-fourth of the volume, we have, 545697 m³ of biogas production. The annual Power Production: 297000 MWh @ Rs. 4.00 per unit (average), the total electricity savings per year is Rs. 118.80 crores. If all waste waters are properly managed only in class I cities in India, we will get Rs. 118.80 crores/year in future through the power production from biogas. The GHG Emission Reductions is calculated as 1315400.1 metric tons per year. Assuming the Carbon Trading price as \$2 per metric tons, we can earn \$ 2630800 per year.

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